





PCT

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

Anslation interna	PATENT COOPER. PC		ATY
MIS INTERNA	ATIONAL PRELIMINA	RY EXAMIN	ATION REPORT
	(PCT Article 36	and Rule 70)	
Applicant's or agent's file reference M63PC011	FOR FURTHER ACTI	ON See Notifi Preliminary	cation of Transmittal of Interna Examination Report (Form PCT/IPEA
International application No. PCT/EP2003/002859	International filing date (a 19 March 2003 (1	-	Priority date (day/month/year) 25 March 2002 (25.03.200
International Patent Classification (IPC) C01F 5/22	or national classification and IF	С	
Applicant	IMB + FRINGS WATER	SYSTEMS GN	ИВН
amended and are the bas 70.16 and Section 607 of These annexes consist of These annexes consist of I Basis of the report contains indications I Priority III Non-establishm IV Lack of unity of V Reasoned state citations and effects VI Certain documents VII Certain defects	sis for this report and/or sheets of the Administrative Instruction of a total of she s relating to the following items: port ment of opinion with regard to not invention ement under Article 35(2) with recognitions supporting such states.	ontaining rectific under the PCT). its.	
Date of submission of the demand	r	ate of completion	n of this report
15 October 2003 (1	15.10.2003)	1	4 June 2004 (14.06.2004)
Name and mailing address of the IPE	A/	uthorized officer	
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International application No.

PCT/EP2003/002859

I. I	I. Basis of the report						
1.	With	regard to	o the elements of the international application:*				
	\boxtimes	the inte	ernational application as originally filed				
	\boxtimes	the desc	cription:	i			
		pages	1-9	, as originally filed			
		pages		, filed with the demand			
		pages	, filed with the letter of				
	\boxtimes	the clai	ims:	1			
		pages	2-20	, as originally filed			
		pages	, as amended (together w	vith any statement under Article 19			
		pages		, filed with the demand			
		pages	1, filed with the letter of	29 March 2004 (29.03.2004)			
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		pages	1/2-2/2	, as originally filed			
		pages		, filed with the demand			
		pages	, filed with the letter of				
	$\prod t$	he seque	ence listing part of the description:				
		pages		, as originally filed			
		pages		, filed with the demand			
		pages	, filed with the letter of				
3.	the in Thes	the land the	nguage of a translation furnished for the purposes of international search (under Rule nguage of publication of the international application (under Rule 48.3(b)). Inguage of the translation furnished for the purposes of international preliminary of	which is: e 23.1(b)). examination (under Rule 55.2 and/ onal application, the international go beyond the disclosure in the			
4.		been f	furnished. amendments have resulted in the cancellation of:				
1		님	the description, pages				
		님	the claims, Nos.				
		LI	the drawings, sheets/fig				
5.	. 🔲	This rebeyond	report has been established as if (some of) the amendments had not been made, sind the disclosure as filed, as indicated in the Supplemental Box (Rule 70.2(c)).**	ce they have been considered to go			
*	in th	lacement his repoi 70.17).	t sheets which have been furnished to the receiving Office in response to an invitat ort as "originally filed" and are not annexed to this report since they do not	tion under Article 14 are referred to contain amendments (Rule 70.16			
*			ment sheet containing such amendments must be referred to under item $\it 1$ and annex	eed to this report.			

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V.	Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability;
	citations and explanations supporting such statement

Statement			
Novelty (N)	Claims	1-20	YES
	Claims		NO
Inventive step (IS)	Claims	1-20	YES
	Claims		NO
Industrial applicability (IA)	Claims	1-20	YES
·	Claims		NO

2. Citations and explanations

1. Reference is made to the following documents:

D1: DE-A-10001493

D2: US-A-5385671

D3: US-A-4865744

2. Novelty

Document D1, which is considered to be the closest prior art, discloses a process for producing magnesium hydroxide from a salt solution. In this process the pH value of a heavy-metal-free solution is increased to 11.5 in order to precipitate the full quantity of dissolved magnesium hydroxide. The magnesium hydroxide is then separated either by mechanical means or using a membrane filter. After a counterflow washing stage with demineralised water, most of which is circulated by reverse osmosis, magnesium hydroxide with a high degree of purity can be obtained (see the drawing and the example).

Document D2 deals with a process for obtaining magnesium hydroxide. The hydroxide is produced by adding sodium lye to a magnesium-containing salt

solution to make it alkaline. The magnesium hydroxide is separated from the dissolved sodium salt by filtering the suspension through a cross-flow membrane (column 2, lines 21 to 55). The permeate is removed.

The subject matter of claim 1 differs from the disclosures of D1 and D2 in that the permeate produced by precipitation of the metal is returned to the cross-flow system.

The process according to **claims 1 to 19** is therefore considered novel (PCT Article 33(2)).

Claim 20 relates to a device for carrying out a process for producing a metal hydroxide from a salt solution. The device described in the present application differs from the devices for carrying out the processes according to D1 and D2 in that it includes at least one line for returning the permeate to a cross-flow filtration unit. The device according to claim 20 is therefore novel.

3. Inventive step

The problem addressed by the present application can therefore be seen as that of providing a process and device for producing a high-purity metal hydroxide in a simple, fast and economical way.

Document D3 describes a process for the continuous workup of aqueous raw material suspensions in a multistage membrane separation unit. The suspension is a dye suspension. The process is characterised by the introduction in each membrane separation stage (n) (where n is a whole number greater than 1) of a dye

suspension (F_n) and wash water (WW_n) , permeate (P_{n+1}) from the subsequent membrane separation stage (n+1) or mixtures of WW_n and P_{n+1} , and separation thereof into a dye suspension (F_{n+1}) and a permeate (P_n) (claim 1). The membrane separation unit works on the principle of ultrafiltration and/or cross-flow microfiltration (claim 7). The cross-flow microfiltration is usually carried out using microporous membranes with pore diameters of 0.1 to 40 μ m, preferably 0.2 to 10 μ m (column 5, lines 3 to 5). It is also possible to add, for example, a reverse osmosis process for further (complete) desalting (column 7, lines 55 to 57).

The solution proposed in **claims 1 to 19** of the present application is considered inventive (PCT Article 33(3)) for the following reasons:

It is known from D1 and D2 to precipitate magnesium hydroxide from a salt solution and to filter the resulting suspension through a cross-flow filter.

It is known from D3 to return the permeate from a cross-flow filter stage to a multistage membrane separation unit in order to reduce the salt content in the suspension. The dye-containing solution is repeatedly purified by the addition of wash water, and thus salts and other impurities are continuously removed from the suspension.

A person skilled in the art would not have adopted the cross-flow filtration process of D3 as a way of solving the aforementioned problem because D3 deals with the continuous purification of a dye suspension. Dye suspensions must have very good suspensibility and must retain good flow properties even when there are

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high concentrations of dye particles in the solution. For this reason the particles in dye suspensions are well suspended and show little or no agglomeration. By contrast, in the present application the magnesium hydroxide is precipitated as voluminous, greasy and slimy agglomerates which are broken up by the claimed process as a result of the high turbulence created, and are prevented from re-forming. A person skilled in the art would therefore not have used the teaching of D3 in order to solve the problem addressed by the present invention.

In the present invention the returning of the permeate to the cross-flow filtration unit results in repeated purification of the metal-hydroxide-containing solution using an ever less salty permeate, which means that any concentration of unwanted impurities can be separated out of the solution.

4. Industrial applicability

The process and device for producing a metal hydroxide with a high degree of purity are clearly industrially applicable.